

MAGIC RESOURCE INVESTORS

COST SHARE PROPOSAL TO DOE

USER-COUPLED CONFIRMATION DRILLING PROGRAM

MARCH 13, 1981

DOE/MRI COST SHARE STRATEGY

- o Current strategy based on geothermal source temperature and flow rate

- o Proposed strategy based on the value of the energy provided by the source for the defined end use

PROPOSED STRATEGY

- o Define the cost of a conventional energy source (natural gas) as the baseline for an unsuccessful well
- o Define the energy cost from the geothermal source necessary to attract an alcohol plant enterprise as a completely successful well
- o Base the degree of success for the project on the final energy cost

DEFINE CONVENTIONAL ENERGY COST = *baseline for unsuccessful well*

o Assumptions

- Natural Gas Boiler Cost = \$120,000^a
- Interest Rate = 18%^b
- Finance Period = 10 years^b
- Natural Gas Cost = \$4.00/10⁶ Btu^c
- Boiler Efficiency = 82.5%^d
- Alcohol Process Thermal Energy Requirements = 65,000 Btu^e
- Alcohol Plant Capacity = 2 million gallons/year^b

o Annual Energy Requirement for Alcohol Production = 130,000 million Btu/year

o Amortized Capital Cost ^(120,000) = \$26,700/year

o Amortized Capital Cost/Annual Energy = \$0.21/million Btu

o Natural Gas Cost = 4.85/million Btu *taking efficiency into account*

o Total Energy Cost = \$5.06/million Btu =

^aRichardson Rapid System

^bClient

^cIntermountain Gas, LV-1

^dChemical Engineering

^eBohler Brothers of America

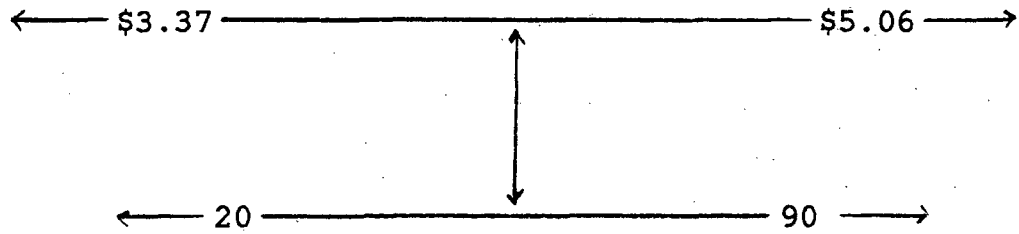
totally unsuccessful cost share

DEFINE ATTRACTIVE ENERGY COST

- o One-third reduction from conventional energy cost is necessary to attract an alcohol enterprise
- o \$3.37 per million Btu

DEGREE OF PROJECT SUCCESS (DOE Cost Share)

Energy Cost (\$/million Btu)



DOE Cost Share (%)

SENARIO I: ASSUMPTIONS

- o 240°F
- o 600 gpm
- o 1,000 feet ^{well} (assumed cost is linear)
- o DOE cost share = 36%

SENARIO I: ECONOMIC CALCULATIONS

o Total Investor Capital Cost

| | | | |
|---|------------------------------|---|----------------|
| - | Well Cost = (\$400,000)(.64) | = | \$ 256,000 |
| - | Ancillary Cost | = | 290,000 |
| - | MTI Equipment Cost | = | <u>900,000</u> |

\$1,446,000

o Amortized Cost (18%, 10 years) \$322,500

o O&M Cost (5% MTI Cost) 45,000

o Electrical Energy (COP = 6.7, \$.025/kW) 141,000

o Total Annual Investor Cost \$508,500

o Cost/Million Btu \$3.91

SENARIO II: ASSUMPTIONS

- o 240°F
- o 600 gpm
- o 3,000 feet
- o DOE cost share = 36%

SENARIO II: ECONOMIC CALCULATIONS

| | | |
|---|--|------------------|
| o | Total Investor Capital Cost | |
| | - Well Cost = $(\$1,200,000)(.64)$ | = \$ 768,000 |
| | - Ancillary Well Cost | = 290,000 |
| | - MTI Equipment Cost | = <u>900,000</u> |
| | | \$1,958,000 |
| o | Amortized Cost (18%, 10 years) | \$436,600 |
| o | O&M Cost (5%) | 45,000 |
| o | Electrical Energy (COP 6.7, \$.025/kW) | <u>141,000</u> |
| o | Total Annual Investor Cost | \$622,600 |
| o | Cost/Million Btu | \$4.79 |

REVISED SENARIO I

- o 240°F
- o 600 gpm
- o 1,000 feet
- o DOE cost share = 40%

o Total Investor Cost = \$1,430,000

o Cost/Million Btu = \$3.88

\$3.88 = 41% DOE cost share

REVISED SENARIO II

- o 240°F
- o 600 gpm
- o 3,000 feet
- o DOE cost share = 60%

o Total Investor Cost = \$1,770,000

o Cost/Million Btu = \$4.30

\$4.30 = 59% DOE cost share

DOE STAKE

| <u>°F</u> | <u>400gpm</u> | <u>600gpm</u> |
|-----------|---------------|---------------|
| 285 | 22% | 20% |
| 275 | | 25% |
| 260 | | 40% |
| 220 | 90% | 85% |
| 210 | 90% | 90% |